



24.4 Unsteady state conduction.

- Unsteady heat transfer.
- Transient heat " "

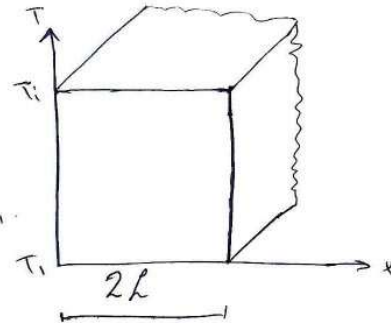
* For plane wall.

$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{q''}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial \tau}$$

In This case temp. is not only a function of x , it is also a function of time. $T(x, \tau)$

* Assumption:

- 1) Infinite plate with thickness $2L$
- 2) T_i is the initial temp @ $T=0.0$
- 3) sudden change while cooling to T_1 .
- 4) constant thermal conductivity.
- 5) Unsteady. (غير مستقر)



$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} + \frac{q''}{k} = \frac{1}{\alpha} \frac{\partial T}{\partial \tau}$$

$$\frac{\partial^2 T}{\partial x^2} = \frac{1}{\alpha} \frac{\partial T}{\partial \tau} \quad \text{--- (1)}$$

$$\theta = T - T_1$$

$$\frac{\partial^2 \theta}{\partial x^2} = \frac{1}{\alpha} \frac{\partial \theta}{\partial \tau}$$

Boundary and initial condition.

$$\theta = \theta_i = T_i - T_1 \quad @ \quad \tau = 0 \quad \text{and} \quad 0 \leq x < 2L$$

$$\theta = 0 \quad @ \quad \tau > 0 \quad x = 0 \quad \text{--- (2)}$$

$$\theta = 0 \quad @ \quad \tau > 0 \quad x = 2L \quad \text{--- (3)}$$



$$\vartheta(x, \tau)$$

$$\vartheta = X(x)H(\tau)$$

$$\frac{\partial \vartheta}{\partial \tau} = X(x) \frac{\partial H}{\partial \tau} \Rightarrow \frac{\partial \vartheta}{\partial x} = H(\tau) \frac{\partial X(x)}{\partial x} \Rightarrow \frac{\partial^2 \vartheta}{\partial x^2} =$$

$$H(\tau) \frac{\partial^2 X(x)}{\partial x^2}$$

$$H(\tau) \frac{\partial^2 X(x)}{\partial x^2} = \frac{1}{\alpha} X(x) \frac{\partial H}{\partial \tau}$$

$$\frac{1}{X(x)} \frac{\partial^2 X(x)}{\partial x^2} = \frac{1}{\alpha} \frac{1}{H(\tau)} \frac{\partial H}{\partial \tau} = -\lambda^2$$

λ^2 : separation parameter

$$\frac{\partial^2 X(x)}{\partial x^2} + \lambda^2 X(x) = 0$$

$$\frac{\partial H}{\partial \tau} + \alpha \lambda^2 H(\tau) = 0$$

$$\vartheta = [c_1 \cos \lambda x + c_2 \sin \lambda x] e^{-\alpha \lambda^2 \tau}$$

$$\text{using B-C} \Rightarrow 0 = (c_1 \cos 0 + c_2 \sin 0) e^{-\alpha \lambda^2 \tau}$$

$$c_1 = 0$$

$$\vartheta = (c_2 \sin \lambda x) e^{-\alpha \lambda^2 \tau} \quad \text{--- (2)}$$

$$\text{using B-C} \Rightarrow 0 = (c_2 \sin 2L\lambda) e^{-\alpha \lambda^2 \tau}$$

$$\sin 2\lambda L = 0$$

$$0, \lambda, 2\pi, 3\pi$$

$$2\lambda L = n\lambda$$

$$\lambda = \frac{n\pi}{2L}$$



$$\lambda = \frac{n\pi}{2L}$$

$$\theta = \sum_{n=1}^{\infty} \left(C_n \sin \frac{n\pi x}{2L} \right) e^{-\alpha \left(\frac{n\pi}{2L} \right)^2 t}$$

substitute in equ. (2).

Infinite plate having thickness... = 2L

$$\frac{T - T_1}{T_1 - T_1} = \frac{\theta}{\theta_i} = \frac{4}{\pi} \sum_{n=1,3,5,7,9,\dots}^{\infty} \frac{1}{n} e^{-\alpha \left(\frac{n\pi}{2L} \right)^2 t} \sin \left(\frac{n\pi x}{2L} \right)$$

صفا الزوايا الراديانية

$\alpha = \frac{\mu}{\rho c}$

4-2 An infinite plate having a thickness of 2.5 cm is initially at a temperature of 150°C, and the surface temperature is suddenly lowered to 30°C. The thermal diffusivity of the material is 1.8 × 10⁻⁶ m²/s. Calculate the center-plate temperature after 1 min by summing the first four nonzero terms of Equation (4-3). Check the answer using the Heisler charts.

thickness = 2L = 2.5 cm, T_i = 150°C, T_s = 30°C
 thermal diffusivity (α) = 1.8 × 10⁻⁶ m²/s, find T | t = 60s
 x = L



calculate the center plate temp. after 1 min. using the first 4 nonzero terms of equation.

Solve:-

$$\frac{T - 30}{150 - 30} = \frac{4}{\pi} \left[\frac{1}{1} e^{-1.8 \times 10^{-6} \times 60 \left[\frac{\pi}{0.0125} \right]^2} \sin \frac{\pi x}{2L} + \frac{1}{3} e^{-1.8 \times 10^{-6} \times 60 \left[\frac{3\pi}{0.0125} \right]^2} \sin \frac{3\pi x}{2L} \right. \\ \left. + \frac{1}{5} e^{-1.8 \times 10^{-6} \times 60 \left[\frac{5\pi}{0.0125} \right]^2} \sin \frac{5\pi x}{2} + \frac{1}{7} e^{-1.8 \times 10^{-6} \times 60 \left[\frac{7\pi}{0.0125} \right]^2} \sin \frac{7\pi x}{2} \right]$$

$$\frac{T - 30}{120} = \frac{4}{\pi} \left[0.1818 - 7.1912 \times 10^{-8} + 6.0834 \times 10^{-20} - 7.27 \times 10^{-38} \right]$$

$$\frac{T - 30}{120} = 0.231 \Rightarrow T = 57.777^\circ\text{C} \quad \#$$



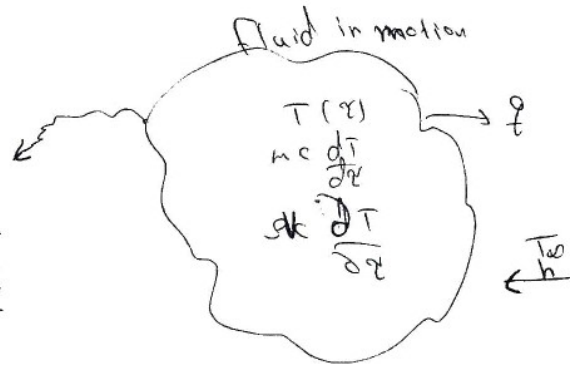
* Lumped - Heat-capacity system.

- The system is assumed to be uniform in Temp. This means that temp difference has been decayed. (متساوية الحرارة)
- The internal thermal conductive resistance is smaller than the external convective resistance.

مخزن حراري متساوي الحرارة

* Energy Balance.

$$\dot{q} = hA(T - T_{\infty}) = -\rho cV \frac{dT}{dt}$$



$V \Rightarrow$ volume

$A \Rightarrow$ surface area

$C \Rightarrow$ specific heat transfer (kJ/kg) - c

$T_{\infty} \Rightarrow$ Temp fluid

$$\frac{T - T_{\infty}}{T_0 - T_{\infty}} = \frac{\theta}{\theta_0} = e^{-\frac{hA}{\rho cV} \tau}$$

$A = m^2$, $T_0 =$ Temp initial

$\tau =$ second $T =$ center temp , $T_{\infty} =$ fluid Temp (air, water)

$c =$ J/kg-e $V = m^3$ $T_0 =$ initial temp

4-6 A piece of aluminum weighing 6 kg and initially at a temperature of 300°C is suddenly immersed in a fluid at 20°C. The convection heat-transfer coefficient is 58W/m²°C. Taking the aluminum as a sphere having the same weight as that given, estimate the time required to cool the aluminum to 90°C, using the lumped-capacity method of analysis.



$m = 6 \text{ kg}$, $T_a = 300^\circ \text{C}$, $T_\infty = 20^\circ \text{C}$, $h = 58 \text{ W/m}^2 \cdot ^\circ \text{C}$.
 Aluminum as a sphere , $T = 90^\circ \text{C}$, find τ (time) using
 lumped-capacity method.

زیر
 sphere \Rightarrow $A = 4\pi r^2$
 $V = \frac{4}{3}\pi r^3$
 Solv_e $\frac{T - T_\infty}{T_a - T_\infty} = e^{-\frac{hA\tau}{\rho c V}}$

from Table A-2 ; Aluminum. $\rho = 2707 \text{ kg/m}^3$
 $c = 0.896 \text{ kJ/kg} \cdot ^\circ \text{C}$
 $(c = 896 \text{ J/kg} \cdot ^\circ \text{C})$

To find volume and Area. we must find (r)
 $\rho = \frac{m}{V}$

$m = \rho V$
 $6 = 2707 \times \frac{4}{3}\pi r^3 \Rightarrow r = 0.0807 \text{ m}$

$A = 4\pi r^2 = 4 \times \pi \times (0.0807)^2 = 0.0822 \text{ m}^2$

$\frac{T - T_\infty}{T_a - T_\infty} = e^{-\frac{hA\tau}{\rho c V}} = e^{-\frac{hA\tau}{cm}}$

$\ln \frac{T - T_\infty}{T_a - T_\infty} = \ln e^{-\frac{hA\tau}{cm}}$

$\ln \frac{90 - 20}{300 - 20} = \frac{-58 \times 0.0822 \times \tau}{896 \times 6}$

$\tau = 1563 \text{ sec}$



4-10 A stainless-steel rod (18% Cr, 8% Ni) 6.4 mm in diameter is initially at a uniform temperature of 25°C and is suddenly immersed in a liquid at 150°C with $h = 120 \text{ W/m}^2 \cdot \text{°C}$. Using the lumped-capacity method of analysis, calculate the time necessary for the rod temperature to reach 120°C.

stainless-steel rod (cylinder) (18% Cr, 8% Ni) $d = 6.4 \text{ mm}$.
 $T_0 = 25$, $T_\infty = 150^\circ\text{C}$, $h = 120$, using lumped-capacity method.

find τ at $T = 120^\circ\text{C}$.
 Sol'n:

From table A-2. (page 651) $\rho = 7817 \text{ kg/m}^3$
 $c = 460 \text{ J/kg}\cdot\text{°C}$
 cylinder.

$$A = \pi dL$$

$$V = \frac{\pi}{4} d^2 L$$

Note: L is unknown. so ... ?

$$\frac{T - T_\infty}{T_0 - T_\infty} = e^{-\frac{hA\tau}{\rho c V}}$$

$$\frac{120 - 150}{25 - 150} = e^{-\frac{120 \times 4 \times \tau}{7817 \times 460 \times 6.4 \times 10^{-3}}}$$

$$\frac{A}{V} = \frac{\pi dL}{\frac{\pi}{4} d^2 L} = \frac{4}{d}$$

L is given

$$\tau = 1316 \text{ sec}$$

* Time constant $\tau_c = \frac{\rho c V}{hA}$

special case IF time is equal to time constant. in lumped capacity method.

$$\frac{\theta}{\theta_0} = e^{-\frac{hA\tau}{\rho c V}} = e^{-\frac{hA}{\rho c V} \left(\frac{\rho c V}{hA}\right)} = e^{-1}$$

$$\frac{\theta}{\theta_0} = 0.368. \quad \therefore T - T_\infty = 36.8\% [T_0 - T_\infty]$$



في جميع الاسئلة السابقة كان السؤال محدد طريقه الحل وهي (lumped). لكن في حاله عدم تحديد طريقه الحل نستخدم biot number لتحديد طريقه الحل.

$$Bi < 0.1 \Rightarrow \text{lumped can be used}$$

$$Bi > 0.1 \Rightarrow \text{from figures (Heisler charts)}$$

$$Bi = \frac{h(V/A)}{k} = \frac{hs}{k}$$

$$s \rightarrow \text{characteristic length. } \frac{V}{A}$$

$$s(\text{plate}) = \frac{V}{A} = \frac{L^3}{L^2} = L$$

$$s(\text{cylinder}) = \frac{V}{A} = \frac{\frac{\pi}{4} d^2 L}{\pi d L} = \frac{d}{4} = \frac{R}{2}$$

$$s(\text{sphere}) = \frac{V}{A} = \frac{\frac{4}{3} \pi R^3}{4 \pi R^2} = \frac{R}{3} = \frac{d}{6}$$

4-16 A 12-mm-diameter aluminum sphere is heated to a uniform temperature of 400°C and then suddenly subjected to room air at 20°C with a convection heat-transfer coefficient of 10 W/m² · °C. Calculate the time for the center temperature of the sphere to reach 200°C.

$$d = 12 \text{ mm. (Aluminum sphere), } T_0 = 400^\circ\text{C, } T_\infty = 20^\circ\text{C}$$

$$h = 10 \text{ W/m}^2 \cdot ^\circ\text{C, } T_1 = 200^\circ\text{C, ?}$$

$$\text{Sol: } \text{Table: } k = 204, \rho = 2707, c = 896.$$

check.

$$\text{sphere } \left(\frac{V}{A}\right) = \frac{d}{6}$$

$$\frac{V}{A} = \frac{d}{6}$$

$$Bi = \frac{h}{k} \frac{V}{A} = \frac{10}{204} \cdot \frac{12 \times 10^{-3}}{6} = 9.8 \times 10^{-5} < 0.1 \Rightarrow \text{lumped can use.}$$

$$\therefore \frac{T - T_\infty}{T_0 - T_\infty} = e^{-\frac{hA\tau}{\rho c V}} \Rightarrow \frac{200 - 20}{400 - 20} = e^{-\frac{10 \times 6 \times \tau}{2707 \times 896 \times 12 \times 10^{-3}}}$$

$$\tau = 362 \text{ sec}$$