

## Unit Operations I (MU0124101) PART 1

Humidification Dehumidification and Cooling Towers

1

### Water-Cooling Tower <sup>1/3</sup>





	ADDRESS OF TAXABLE PARTY.	ADDRESS OF TAXABLE PARTY.	







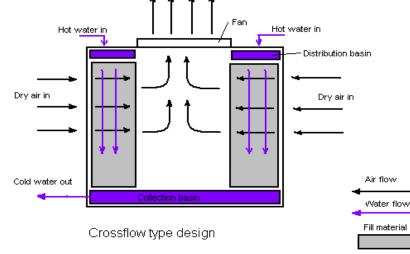
### Water-Cooling Tower <sup>2/3</sup>

Warm water flows counter-currently to an air stream. The warm water enters the top of a packed tower and cascades down through the packing, leaving at the bottom.

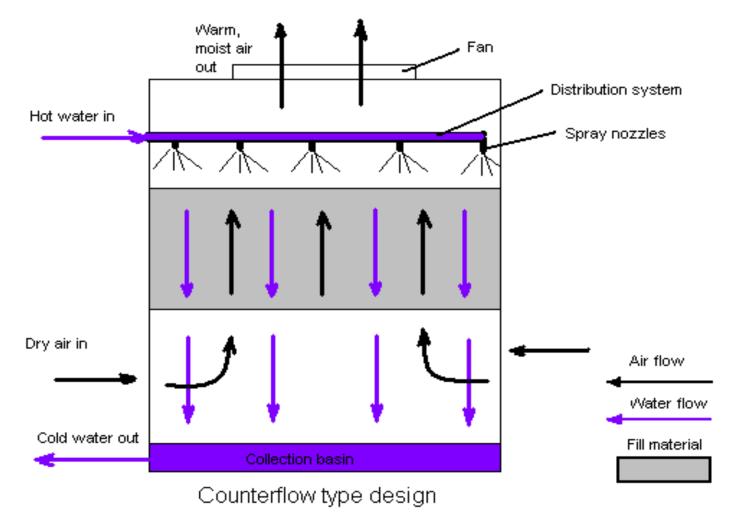
Air enters at the bottom of the tower and flows upward through the descending water by the natural draft or by the action of a fan.

\*The water is distributed by troughs and overflows to cascade over slat gratings or packing that provide large interfacial areas of contact between the water and air in the form of droplets and film of water.

The tower packing often consists of slats of wood or plastic or of a packed bed.  $\uparrow \uparrow \uparrow \uparrow^{Moist, warm air out}$ 



### Water-Cooling Tower <sup>3/3</sup>



# Theory and Calculation of Water-Cooling Towers

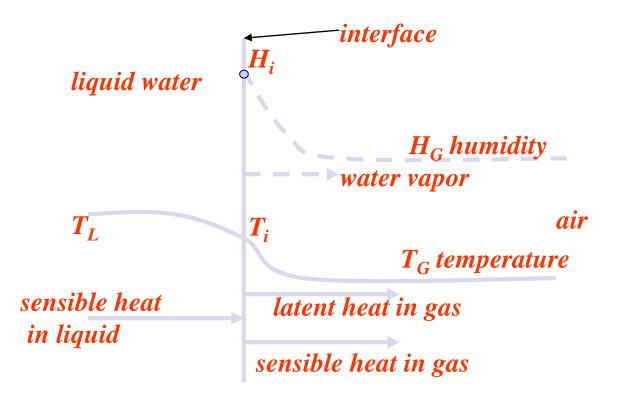


Figure 10.5-1: Temperature and concentration profile in upper part of cooling tower.

### Vapor Pressure of Water & Humidity

#### Introduction

- calculation involve properties and concentration of mixtures of water vapor and air.
- Humidification
  - transfer of water from the liquid phase into a gaseous mixture of air and water vapor.
- Dehumidification
  - reverse transfer where the water vapor is transferred from the vapor state to the liquid state.

### Humidity & Humidity Chart <sup>1/5</sup>

(1) <u>Humidity, H</u>: the kg of water vapor contained in 1 kg of dry air.

$$H = \frac{18.02}{28.97} \frac{p_A}{P - p_A}$$

where,

 $p_A$  = partial pressure of water vapor in the air. Saturated air – water vapor in equilibrium with liquid water.

$$p_A = p_{AS}$$
  $H_S = \frac{18.02}{28.97} \frac{p_{AS}}{P - p_{AS}}$ 

where,

 $p_{AS}$  = saturated vapor pressure.

### Humidity & Humidity Chart <sup>2/5</sup>

#### 2. Percentage humidity H<sub>p</sub>

The percentage humidity  $H_P$  is defined as 100 times the actual humidity H of the air divided by the humidity  $H_S$  if the air were saturated at the same temperature and pressure:

Equation 9.3-3 
$$H_P = 100 \frac{H}{H_S}$$

#### 3. Percentage relative humidity $H_R$

The amount of saturation of an air–water vapor mixture is also given as percentage relative humidity  $H_R$  using partial pressures:

Equation 9.3-4

$$H_R = 100 \frac{p_A}{p_{AS}}$$

### Humidity & Humidity Chart <sup>3/5</sup>

#### (4) Humid volume, $v_H$

It can be defined as total volume (m<sup>3</sup>) of 1 kg of dry air plus the vapor it contains at 1 atm abs pressure and the given gas temp.

 $v_H (m^3/kg \, dry \, air) = (2.83 \, x \, 10^{-3} + 4.56 \, x \, 10^{-3} \, H) \, T (K).$ 

#### (5) Total enthalpy of an air-water mixture, $H_Y$

- the total enthalpy of 1 kg of air plus its water vapor.

- sensible heat of the air-water vapor mixture plus the latent heat.

#### $H_Y(kJ/kg \ dry \ air) = (1.005 + 1.88 \ H) \ (T \ ^oC-0) + 2501.4H$

where,

 $T_{ref}$  for both components = 0 °C

### Humidity & Humidity Chart <sup>4/5</sup>

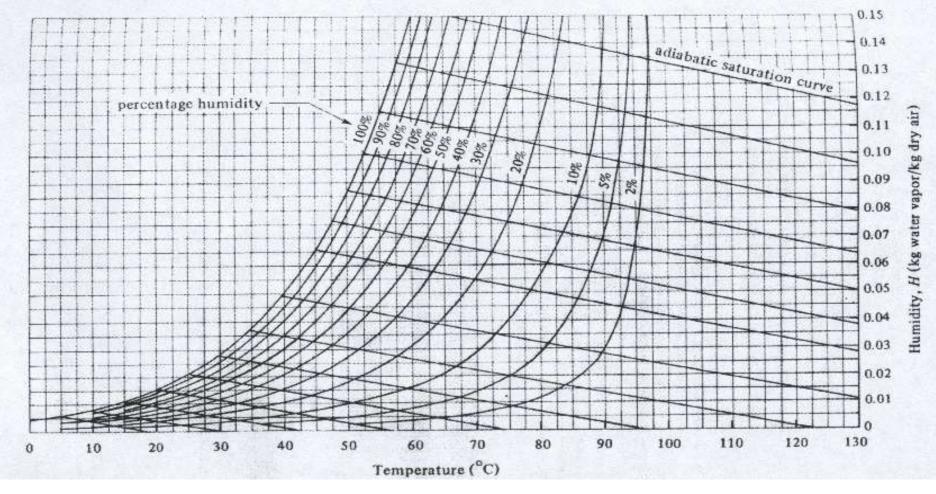
#### 6. Humid heat

The humid heat c<sub>s</sub> is the amount of heat in J (or kJ) required to raise the temperature of 1 kg of dry air plus the water vapor present by 1 K or 1°C. The heat capacity of air and water vapor can be assumed constant over the temperature ranges usually encountered at 1.005 kJ/kg dry air • K and 1.88 kJ/kg water vapor • K, respectively. Hence, for SI and English units,

Equation 9.3-6

 $c_S \, \text{kJ/kg dry air} \cdot \text{K} = 1.005 + 1.88H$  (SI)  $c_S \, \text{btu/lb}_m \, \text{dry air} \cdot ^\circ \text{F} = 0.24 + 0.45H$  (English)

### Humidity & Humidity Chart <sup>5/5</sup> Humidity Chart



### Example 9.3-1 <sup>1/2</sup> Use of Humidity Chart

Air entering a dryer has a temperature (dry bulb temperature) of  $60^{\circ}$ C and a dew point of 26.7°C. Using the humidity chart, determine the actual humidity H, percentage humidity H<sub>P</sub>, humid heat c<sub>S</sub>, and humid volume v<sub>H</sub> in SI units.

The difference between dewpoint and wet bulb temperature is that dewpoint temperature is the temperature to which we should cool the air to saturate the air with water vapor whereas wet bulb temperature is the temperature that we get from a moistened thermometer bulb that is exposed to air flow

Solution: The dew point of 26.7°C is the temperature when the given mixture is at 100% saturation. Starting at 26.7°C (Fig. 9.3-2), and drawing a vertical line until it intersects the line for 100% humidity, a humidity of  $H = 0.0225 \text{ kg H}_2\text{O/kg}$  dry air is read off the plot. This is the actual humidity of the air at 60°C. Stated in another way, if air at 60°C and having a humidity H = 0.0225 is cooled, its dew point will be 26.7°C.

### Example 9.3-1 <sup>2/2</sup>

Locating this point where H = 0.0225 and  $t = 60^{\circ}C$  on the chart, the percentage humidity  $H_P$  is found to be 14%, by linear interpolation vertically between the 10 and 20% lines. The humid heat for H = 0.0225 is, from Eq. (9.3-6),

$$c_S \,\text{kJ/kg} \,\text{dry} \,\text{air} \cdot \text{K} = 1.005 + 1.88H$$
 (SI)

$$c_s = 1.005 + 1.88(0.0225)$$

= 1.047 kJ/kg dry air  $\cdot$  K or 1.047  $\times$  10<sup>3</sup> J/kg  $\cdot$  K

The humid volume at  $60^{\circ}$ C (140°F), from Eq. (9.3-7), is

$$v_H \,\mathrm{m}^{3/\mathrm{kg}} \,\mathrm{dry} \,\mathrm{air} = (2.83 \times 10^{-3} + 4.56 \times 10^{-3} \,H)T \,\mathrm{K}$$
  
 $v_H = (2.83 \times 10^{-3} + 4.56 \times 10^{-3} \times 0.0225)(60 + 273)$   
 $= 0.977 \,\mathrm{m}^{3/\mathrm{kg}} \,\mathrm{dry} \,\mathrm{air}$