

**Example Problem 1.1:** Calculate the mass concentration of 2 gram moles of sulphur dioxide to be used to manufacture sulfuric acid in a 0.20 m<sup>3</sup> of reactor.

**Solution 1.1:** 2 moles of sulphur dioxide is equal to  $64 \times 2 \text{g} = 128 \text{g}$

So mass concentration is  $128 \text{g}/0.20 \text{m}^3 = 128 \times 0.001 \text{kg}/0.20 \text{m}^3 = 0.64 \text{kg/m}^3$

**Example Problem 1.2:** A mixture of noble gases [helium, argon, krypton, and xenon] is at a total pressure of 100 kPa and a temperature of 200 K. If the mixture has equal kmole fractions of each of the gases, determine:

- a) The composition of the mixture in terms of mass fractions.
- b) Total molar concentration
- c) The mass density.

### **Solution 1.2:**

(a) Let 100 kmol of the mixture

Molecular weight of helium, argon, krypton (3), and xenon (4) are 4, 40, 83.8 and 131.3 kg/mol respectively.

Moles of each component of the mixture = 25 moles

So total mass of mixture =  $25 \times 4 + 25 \times 40 + 25 \times 83.8 + 25 \times 131.3 = 6477.5$  kg

So mass fractions (component mass/ Total mass) are:

$$\text{Helium} = 25 \times 4 / 6477.5 = 0.015,$$

$$\text{Argon} = 25 \times 40 / 6477.5 = 0.154,$$

$$\text{Krypton} = 25 \times 83.8 / 6477.5 = 0.323 \text{ and}$$

$$\text{Xenon} = 25 \times 131.3 / 6477.5 = 0.507$$

The average molecular weight of the mixture = total mass/100 kmol = 6477.5 kg/100 kmol = 64.775 kg/kmol = 0.064775 kg/mol

(b) Temperature  $T = 200$  K, Pressure  $P = 100$  kPa,  $R = 8.314$  kPa.m<sup>3</sup>.kmol<sup>-1</sup>.K<sup>-1</sup>.

So Total molar concentration,  $C = P/RT = 60.14$  mol/m<sup>3</sup>.

(c) Mass density = Total molar concentration (C)  $\times$  average molecular weight of the mixture =  $60.14$  mol/m<sup>3</sup>  $\times$   $0.064775$  kg/mol =  $3.896$  kg/m<sup>3</sup>.

## 1.2.2 Fluxes

The flux is defined as the rate of transport of species  $i$  per unit area in a direction normal to the transport. The flux is calculated with respect to a fixed reference frame. The molar flux of species  $i$  can be represented as

$$N_{i-mol} = C_i u_i \quad (1.10)$$

Here  $N_{i-molar}$  is the molar flux of species  $i$  and  $u_i$  is the velocity of  $i$  with respect to a fixed reference frame. In the same fashion, a mass flux,  $N_{i-mass}$  can be represented as

$$N_{i-mass} = \rho_i u_i \quad (1.11)$$

The units of the molar and mass fluxes are moles/m<sup>2</sup>.s and mass/m<sup>2</sup>.s. Sometimes it is convenient to interpret the total flux of species  $i$  with respect to an arbitrary reference frame rather than a fixed set of reference frame. The molar flux of species  $i$  based on arbitrary reference velocity  $u_0$  is denoted by  $J_{i-mol}$  which can be defined as

$$J_{i-mol} = C_i (u_i - u_0) \quad (1.12)$$

Similarly mass flux of species  $i$  based on arbitrary reference velocity  $u_0$  is denoted by  $J_{i-mass}$  which can be expressed as

$$J_{i-mass} = \rho_i (u_i - u_0) \quad (1.13)$$

In a system, since several molecular species move with different average velocities, a frame of moving reference must be chosen. The important moving references are mass average, molar average and volume average velocities.

## ***Mass-average velocity***

The mass average velocity can be defined in terms of the mass concentration and the velocity of species  $i$  based on fixed axis. It is expressed as

$$U_{mass} = \frac{\sum_{i=1}^n \rho_i u_i}{\sum_{i=1}^n \rho_i} \quad (1.14)$$

### ***Molar average velocity***

The molar average velocity can be expressed by the expression analogous to the mass average velocity. It can be represented by replacing mass concentration of species  $i$ ,  $\rho_i$  with molar concentration of species  $i$ ,  $C_i$  :

$$U_{mol} = \frac{\sum_{i=1}^n C_i u_i}{\sum_{i=1}^n C_i} \quad (1.15)$$

### ***Volume average velocity***

For experimental analysis the volume average velocity is important due to a fixed system of constant volume. The volume average velocity can be expressed by

$$U_{vol} = \sum_{i=1}^n \bar{v}_i C_i u_i \quad (1.16)$$

where  $\bar{v}_i$  is the partial molar volume of species  $i$ .

## **Relation between fluxes**

One can obtain the molar flux of  $i$  expressed in Equation (1.12) with respect to the molar average velocity as

$$J_{i-mol} = C_i (u_i - U_{mol}) \quad (1.17)$$

Substituting the Equation (1.10) into the Equation (1.17) and rearranging gives

$$N_{i-mol} = J_{i-mol} + C_i U_{mol} \quad (1.18)$$

Again substituting the definition of molar average velocity defined in Equation (1.15) into the Equation (1.18) we get

$$N_{i-mol} = J_{i-mol} + C_i \frac{\sum_{i=1}^n C_i u_i}{\sum_{i=1}^n C_i} \quad (1.19)$$

Or

$$N_{i-mol} = J_{i-mol} + x_i \sum_{i=1}^n N_{i-mol} \quad (1.20)$$



For binary system of component A and B,  $\sum_{i=1}^n N_{i-mol} = N_A + N_B = N$ . Therefore the

Equation (1.20) can be written for binary system as

$$N_{A-mol} = J_{A-mol} + x_A N \quad (1.21)$$

**Example Problem 1.3:** One kmole of gas mixture at a total pressure of 250 kPa and 303 K contains 10% CH<sub>4</sub>, 30% C<sub>2</sub>H<sub>6</sub>, and 60% H<sub>2</sub> by volume. The absolute velocities of each species are -10 m/s, -5 m/s, and 15 m/s, respectively, all in the direction of the z-axis.

(a) Determine the molar average velocity,  $U_{mol}$  for the mixture.

(b) Evaluate the four fluxes:  $J_{CH_4-mol}$ ,  $N_{CH_4-mol}$ .

**Solution 1.3:**

$$(a) U_{mol} = \frac{\sum_{i=1}^n C_i u_i}{\sum_{i=1}^n C_i} = \sum_{i=1}^n y_i u_i = (0.1)(-10) + (0.30)(-5) + (0.60)(15) = 6.5 \text{ m/s}$$

$$(b) C = P/RT = 250/(8.314 \cdot 303) = 0.09924 \text{ kmol/m}^3 = 99.24 \text{ mol/m}^3$$

$$C_{CH_4} = 0.10 \cdot 99.24 \text{ mol/m}^3 = 9.924 \text{ mol/m}^3$$

$$J_{CH_4-mol} = C_{CH_4} (u_{CH_4} - U_{mol}) = (9.924) \cdot (-10 - 6.5) = -163.746 \text{ mol/m}^2\text{s}$$

$$N_{CH_4-mol} = J_{CH_4-mol} + C_{CH_4} U_{mol} = -163.746 + 9.924 \cdot 6.5 \text{ mol/m}^2\text{s} = -99.24 \text{ mol/m}^2\text{s}$$

References:

1. Treybal, R. E., "Mass-Transfer Operations", 3<sup>rd</sup> Edition, McGraw-Hill, 1981
2. Geankoplis, C.J., "Transport Processes and Separation Process Principles". 4<sup>th</sup> Edition, Prentice-Hall of India, New Delhi, 2005.
3. Dutta, B.K., "Principles of Mass transfer and Separation Processes". Prentice-Hall of India, New Delhi, 2007.



