



Republic of Iraq
Ministry of Higher Education
and Scientific Research
Al-Mustaqbal University College
Chemical Engineering and Petroleum Industries
Department

Subject: Oil and Gas Field Processing
3rd Class

Lecture 6

Crude Oil Distillation

The process of distillation is the most common method adopted for separating the constituents of crude oil into compounds or groups of compounds having industrial uses. Crude oil consists of a complex mixture of hydro-carbons widely differing in boiling points. Distillation is done to separate the crude oil into the basic fractions like motor gasoline kerosene, gas oil and fuel oil.

1. Atmospheric Distillation

Crude distillation unit (CDU) is the first and most fundamental step in the refining process, also known as topping unit, or atmospheric distillation unit. The primary purpose of the atmospheric distillation tower is to separate crude oil into its components (or distillation cuts, distillation fractions) for further processing by other processing units. It receives high flow rates hence its size and operating cost are the largest in the refinery. The capacity of the CDU ranges from 10,000 barrels per stream day (BPSD) to 400,000 BPSD. The economics of refining favours larger units. A good size CDU can process about 200,000 BPSD.

These towers can be up to 150 feet (50 meters) high and contain 20 to 40 fractionation trays spaced at regular intervals. Before entering the column distillation, desalted crude oil pass through a network of pre-heat exchangers in order to heat it initially with hot material drawn from the bottom of the distillation tower to raise its temperature up to 450°F and then to a heating furnace, which brings the temperature up to about 650°F. This part of process is essential because the carbon will be deposited inside the pipes and equipment through which it flows when the oil gets much hotter. The hot crude oil enters the column distillation and most of it vaporizes. Unvaporized heavy oil cuts and residue will drop to the bottom of the column, where it is drawn off. Inside the tower distillation column,

there are the so-called trays, which are working mainly in the separation of crude oil to light the required derivatives. These trays permit the vapors from below to pass from it and contact with the condensed liquid on top of the tray that provides excellent contact between vapor and liquid. Condensed liquid flows down through a pipe to the hotter tray below, where the higher temperature causes re-evaporation. A given molecule evaporates and condenses many times before finally leaving the tower. Products are collected from the top, bottom and side of the column. In modern towers, a portion of the condensed overhead liquid product from a distillation tower that is returned to the upper part of the tower, this **reflux** plays a major role in controlling temperature at the top of the tower and further enhance separation.

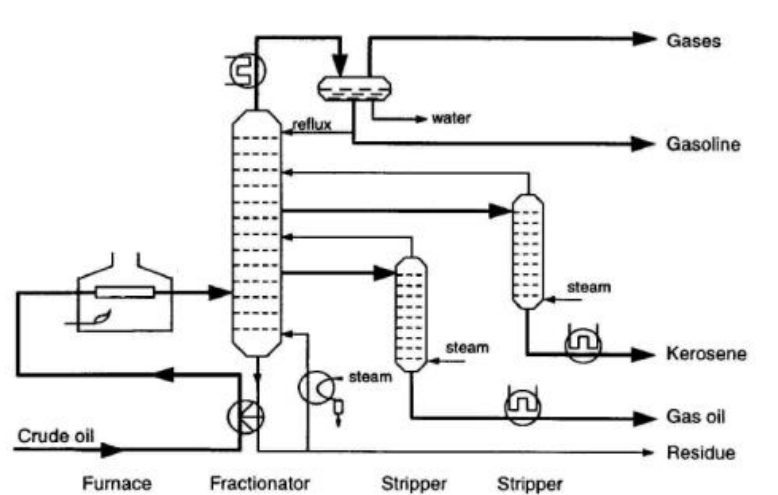


Figure 5.1: Atmospheric Distillation

Fractionation process depends on :

1- Number of Trays 2- Reflux ratio 3- Quantity of steam added to the column

As increasing in trays no. and reflux ratio, the efficiency of separation process is increasing.

Products from ADU

The light products, which have low boiling points, tend toward the top and the heavier products, with relatively higher boiling points tend toward the bottom. The product obtained from a top of ADC under atmospheric pressure is gasoline (C_5 to C_8). This fraction withdrawal as a vapor then is condensed and a part of it will be returned to the atmospheric column as a reflux.

Other products will withdrawal from several points along atmospheric column as a liquid. These products are cooled and a part of them will be returned to the column as a reflux and the remaining parts send to the stripper towers (small fractionating column like column distillation having 4-8 trays placed on each other – beside the distillation column). These stripper towers are aimed to remove the light compounds that effect on the flash point.

The other products are: Heavy straight naphtha, Kerosene, & Light gas oil.

The remaining part at the bottom of atmospheric distillation will be sent to the vacuum distillation tower.

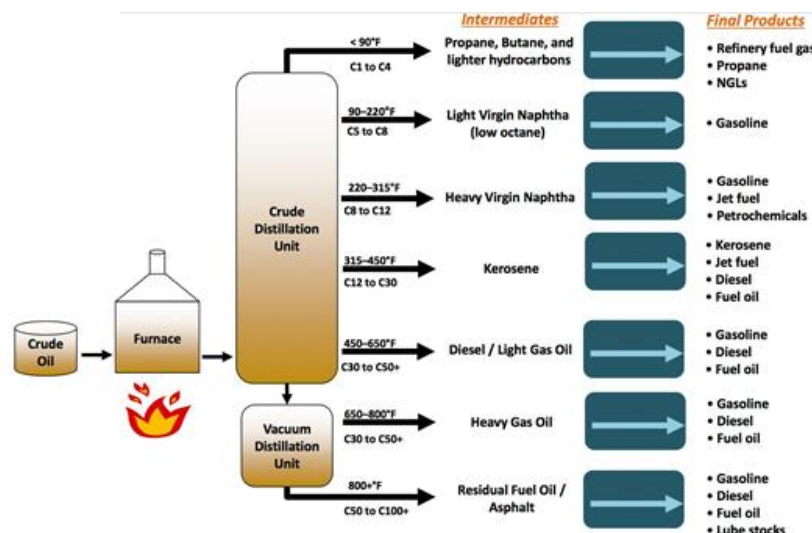


Figure 5.2 Products from Crude distillation unit.

2. Vacuum Distillation Column

The residue from an atmospheric distillation tower can be sent to a vacuum distillation tower, which recovers additional liquid. The furnace outlet temperatures required for atmospheric pressure distillation of the heavier fractions of crude oil are so high that thermal cracking would occur, with the resultant loss of product and equipment fouling. These materials are therefore distilled under vacuum because the boiling temperature decreases with a lowering of the pressure. Distillation is carried out with absolute pressures in the tower flash zone area of 25 to 40 mmHg (Fig. 23). To improve vaporization, the effective pressure is lowered even further (to 10 mmHg or less) by the addition of steam to the furnace inlet and at the bottom of the vacuum tower. Addition of steam to the furnace inlet increases the furnace tube velocity and minimizes coke formation in the furnace as well as decreasing the total hydrocarbon partial pressure in the vacuum tower.

The main products from this unit are:

- 1- Heavy gas oil
- 2- Lubricant
- 3- Asphalt or vacuum residue (B.P > 1000F)

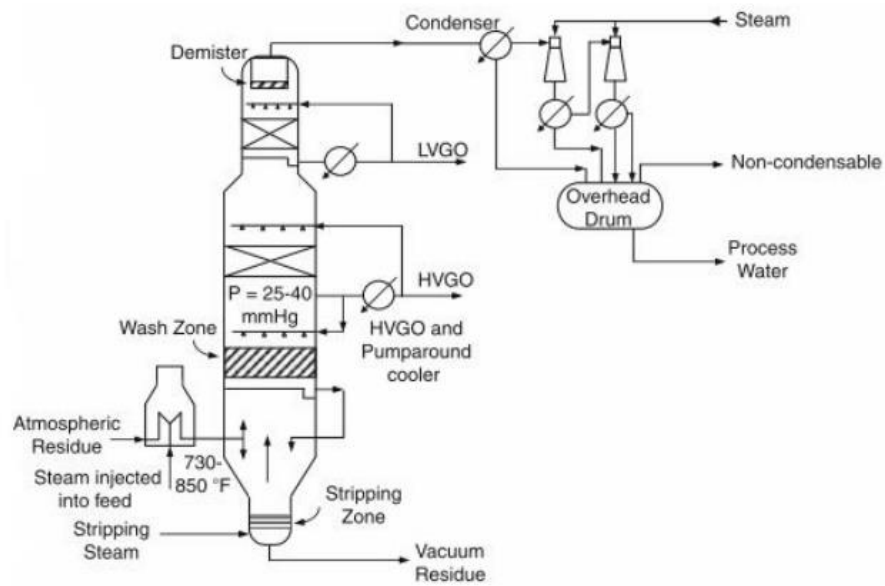


Figure 5.3 Process flow diagram of the vacuum distillation unit.